

The Influence of Various Variables on In Situ Transesterification of *J. curcas*

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Process Intensification Group

Bionergy III, May 22 - 27, 2011

Methyl Ester



- METHYL ESTER (BIODIESEL)
 - Renewable fuel for diesel engines derived from natural oils which meet the specification (ASTM D 6751, EN 14214)
 - Composed of fatty acids alkyl ester
 - Transported and sold using existing infrastructure



Methyl Ester



- 4 factors determining biodiesel competitiveness as fuel
 - Feedstock price
 - Biodiesel production cost
 - Policy (tax, incentive) on biodiesel
 - Crude oil prices



Methyl Ester

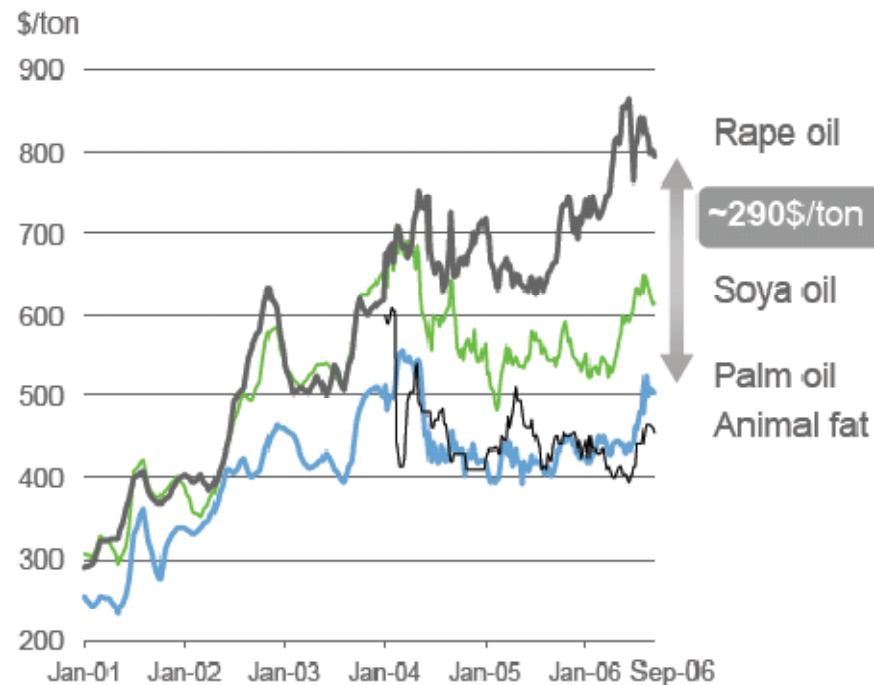
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Feedstock Price

(Edible oil)

Price development of different feedstocks
Jan 2001 - Sep 2006



Source: Oil World

Source: Kimmo Rahkamo, Neste Oil presentation material

Methyl ester

Feedstock
price

Biodiesel
production

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flowchart

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Feedstock Price



Fatty acid composition in various non edible oils (Azam *et al.*, 2005)

| Fatty acid | | <i>J.curcas</i> | <i>P. pinnata</i> | <i>S. oleidis</i> | <i>A. indica</i> |
|------------|------|-----------------|-------------------|-------------------|------------------|
| Capric | 10:0 | | | 0.8 | |
| Lauric | 12:0 | | | 35.6 | |
| Myristic | 14:0 | 1.4 | | 50.7 | |
| Palmitic | 16:0 | 15.6 | 10.6 | 4.5 | 14.9 |
| Stearic | 18:0 | 9.7 | 6.8 | | 14.4 |
| Oleic | 18:1 | 40.8 | 49.4 | 8.3 | 61.9 |
| Linoleic | 18:2 | 32.1 | 19 | 0.1 | 7.5 |
| Arachidic | 20:0 | 0.4 | 4.1 | | 1.3 |
| Eicosenoic | 20:1 | | 2.4 | | |
| Behinic | 22:0 | | 5.3 | | |
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Methyl ester

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Methyl ester

Feedstock
price

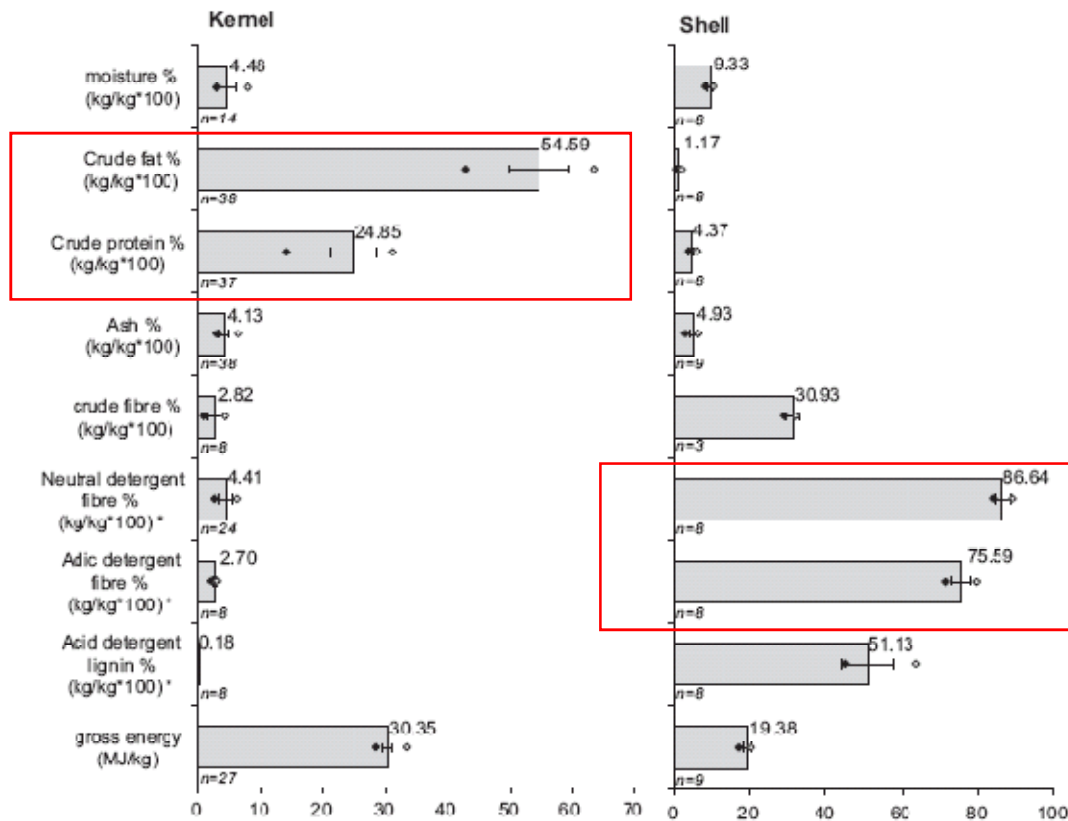
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- The kernel contains mostly fat and protein while the shell dominates by fiber
- Oil content varies very much, but generally between 30 – 60%



- Problems (1):

- Via conventional TE, when alkali catalyst is employed, high FFA contents in the JC oil promotes saponification rather than TE reaction and produce soap rather than methyl ester



FFA

Soap

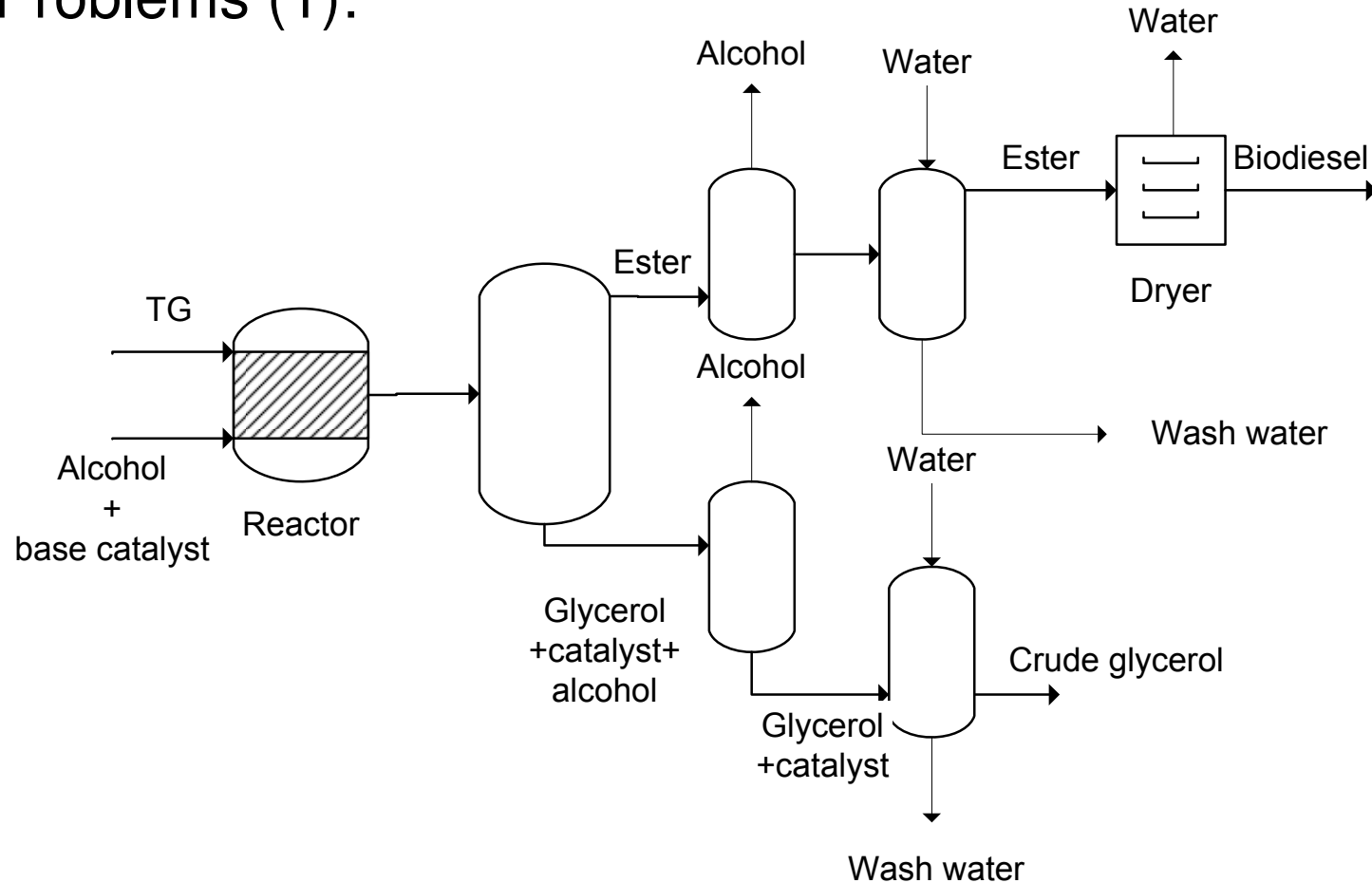
Water

- Consume the catalyst and halt the TE process. Effect on yield as well as on downstream processing



Conventional T.E

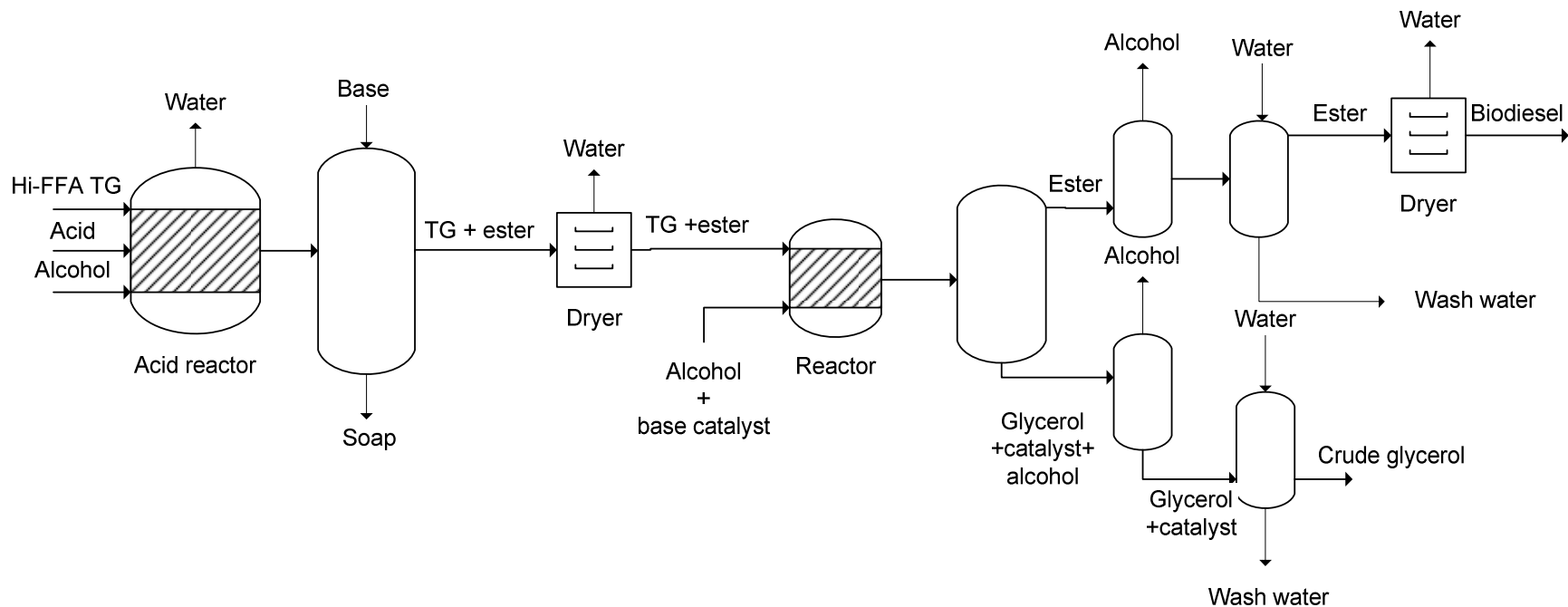
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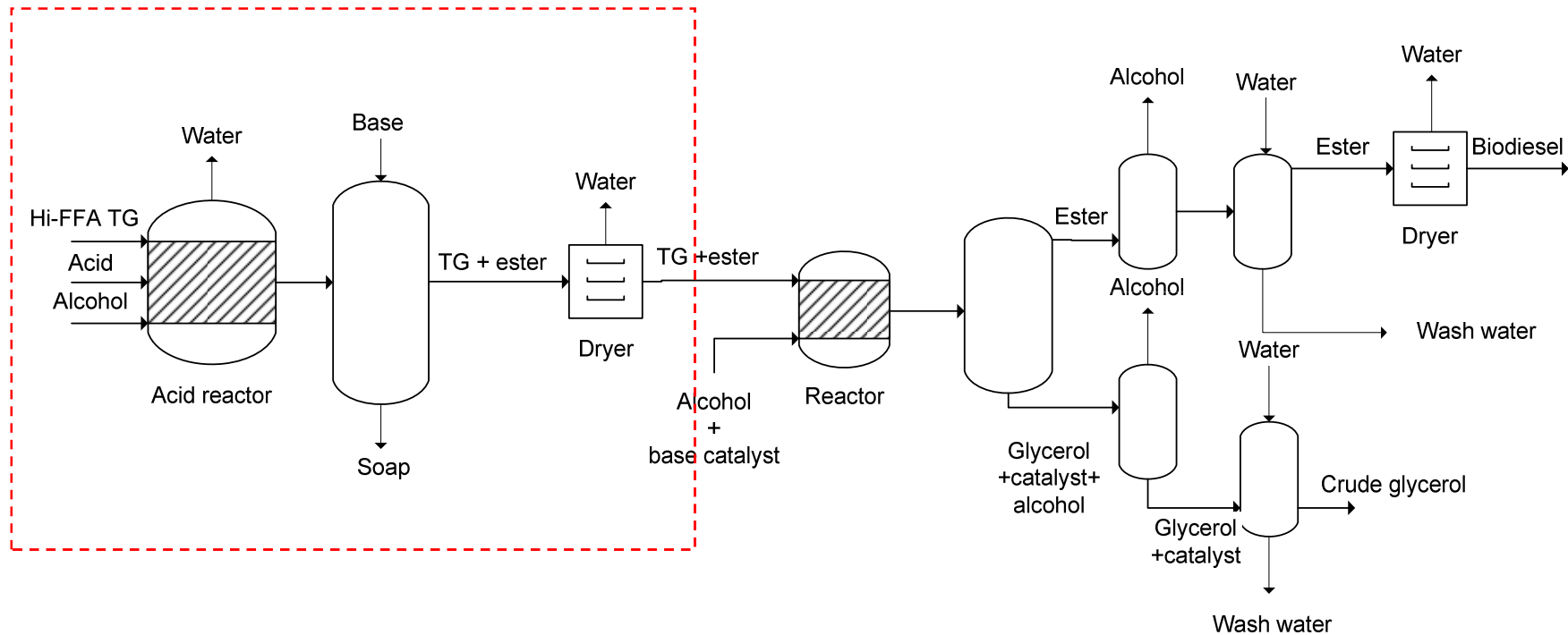
Conventional TE with high FFA raw material

- Problems (1):



Conventional TE with high FFA raw material

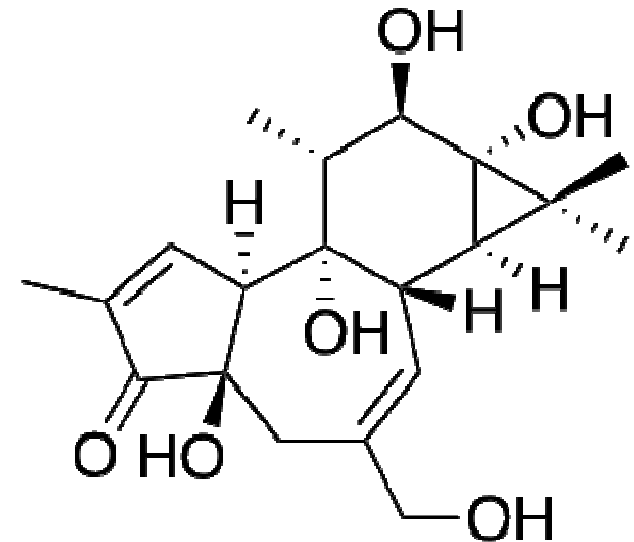
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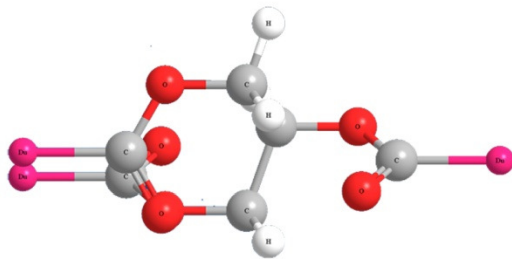
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PROBLEM 2

- Phorbol esters in JC are toxic, even in low concentration
- The phorbol esters end up in the meal, make the meal unsuitable for animal feed
- There is a report that phorbol esters decompose in access methanol, but there is no report on the fate of phorbol esters in in situ transesterification of JC



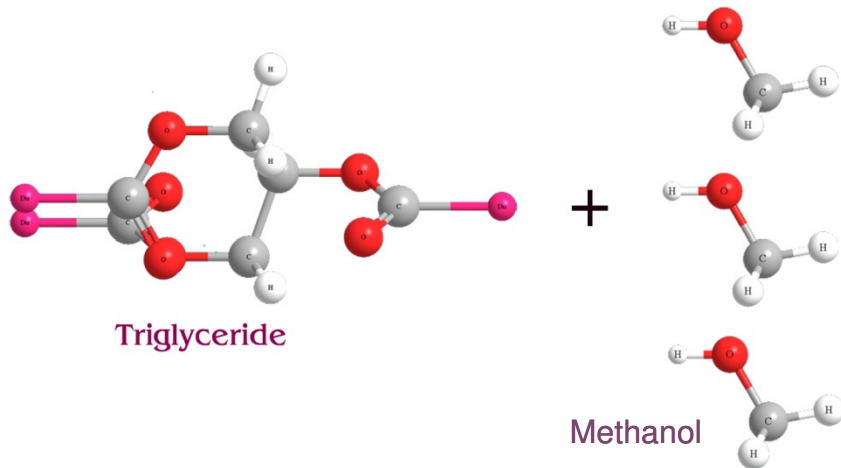
Biodiesel Production



Triglyceride



Biodiesel Production



Methyl ester

Feedstock
price

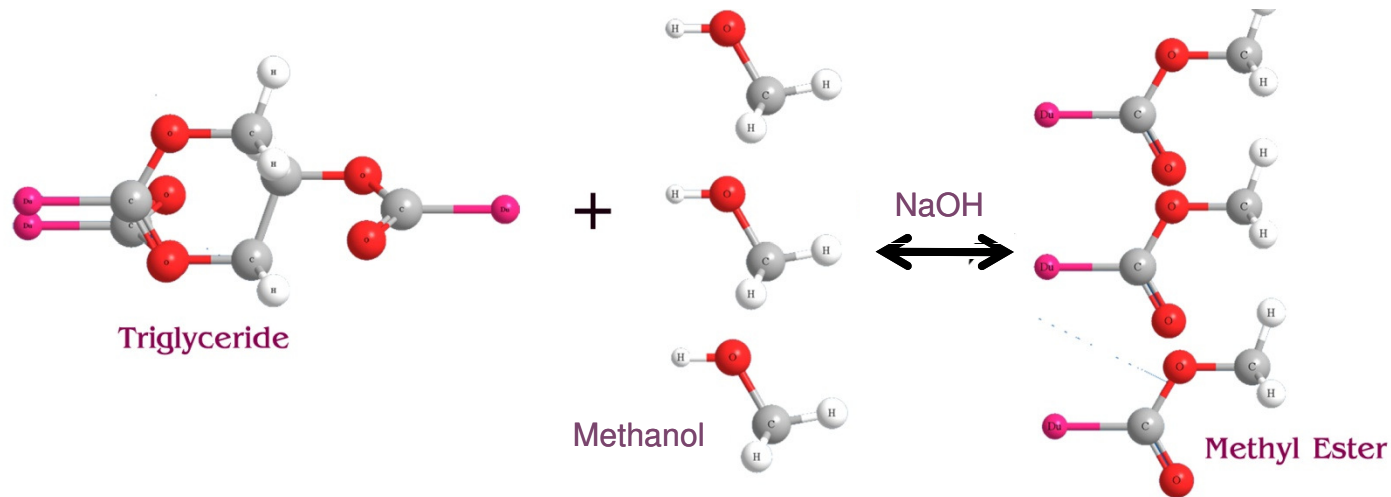
Biodiesel
production

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Biodiesel Production



Methyl ester

Feedstock
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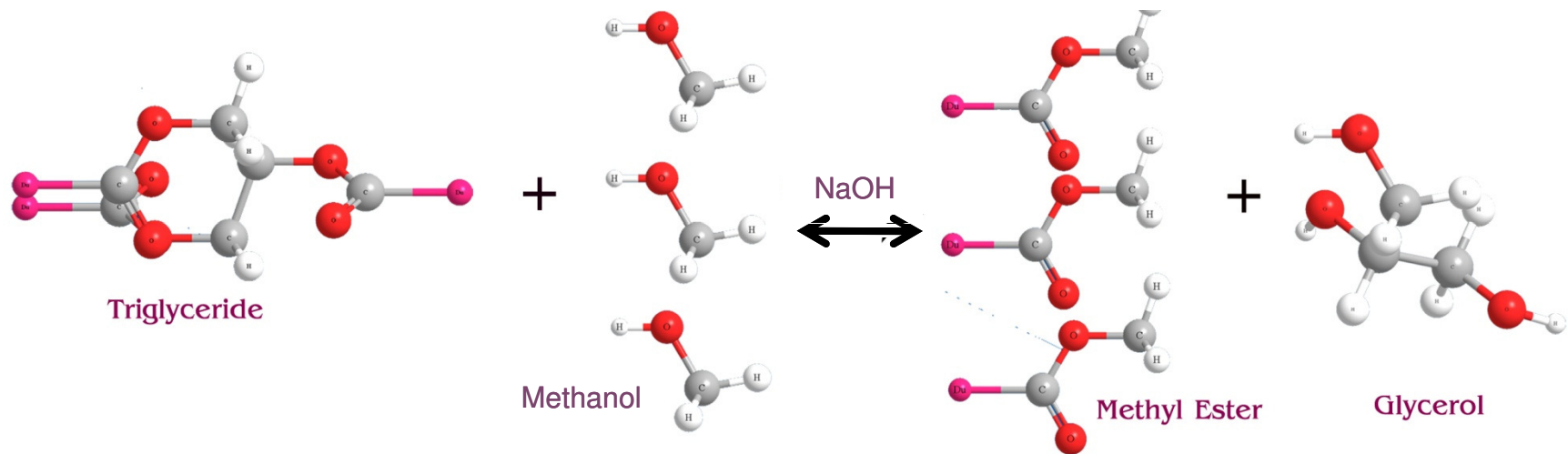
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Methyl ester

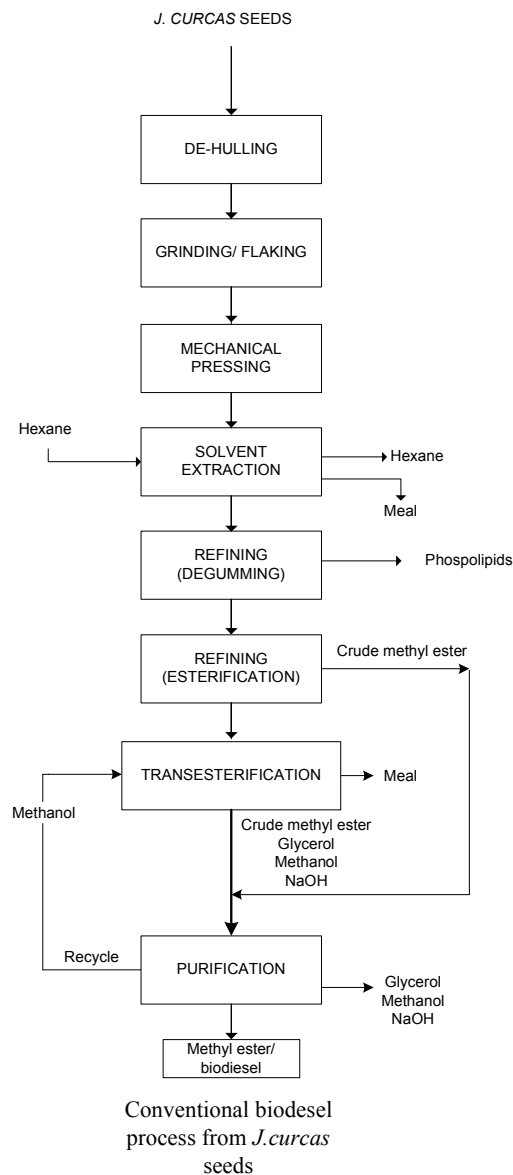
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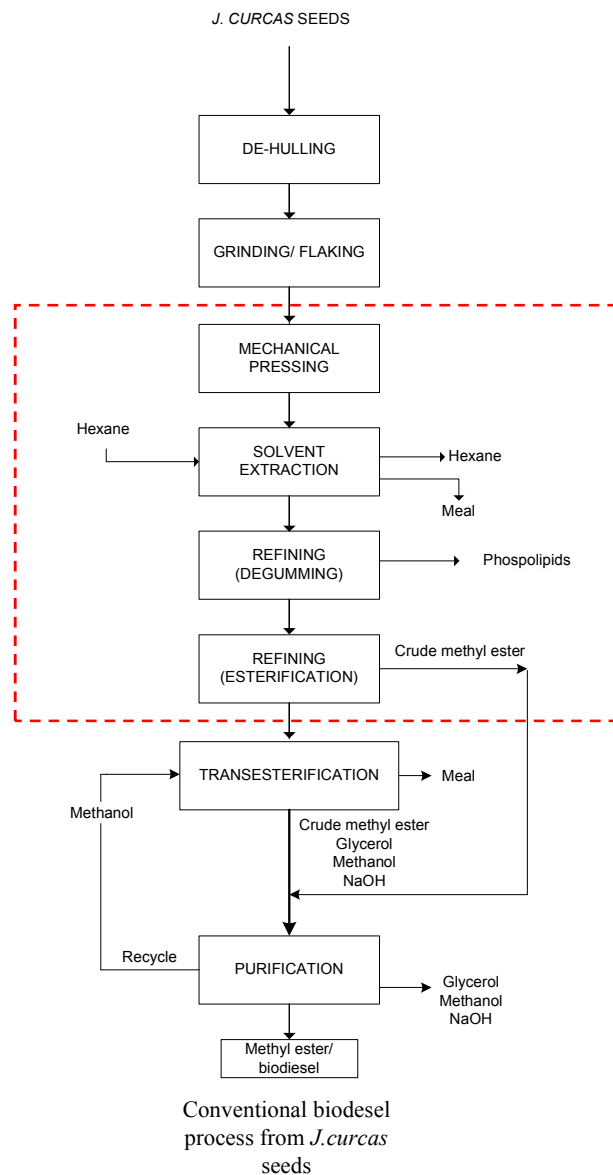
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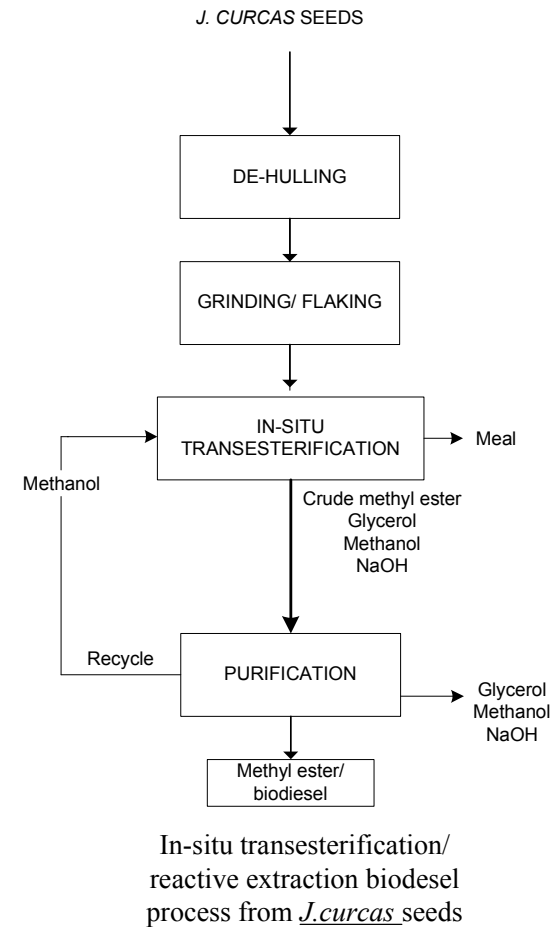
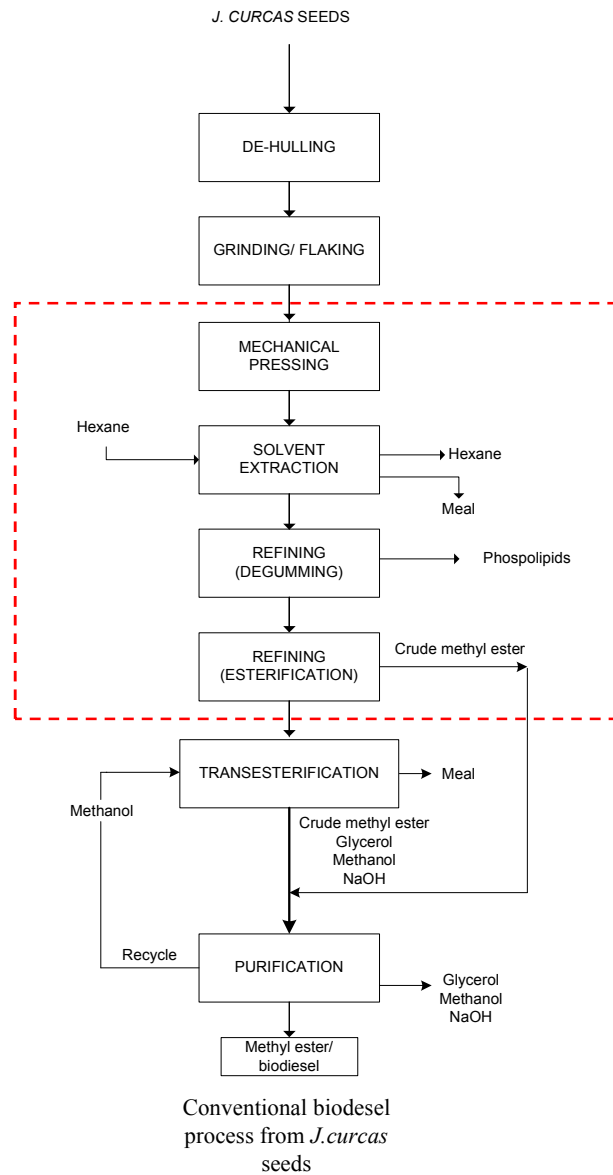
Conclusion

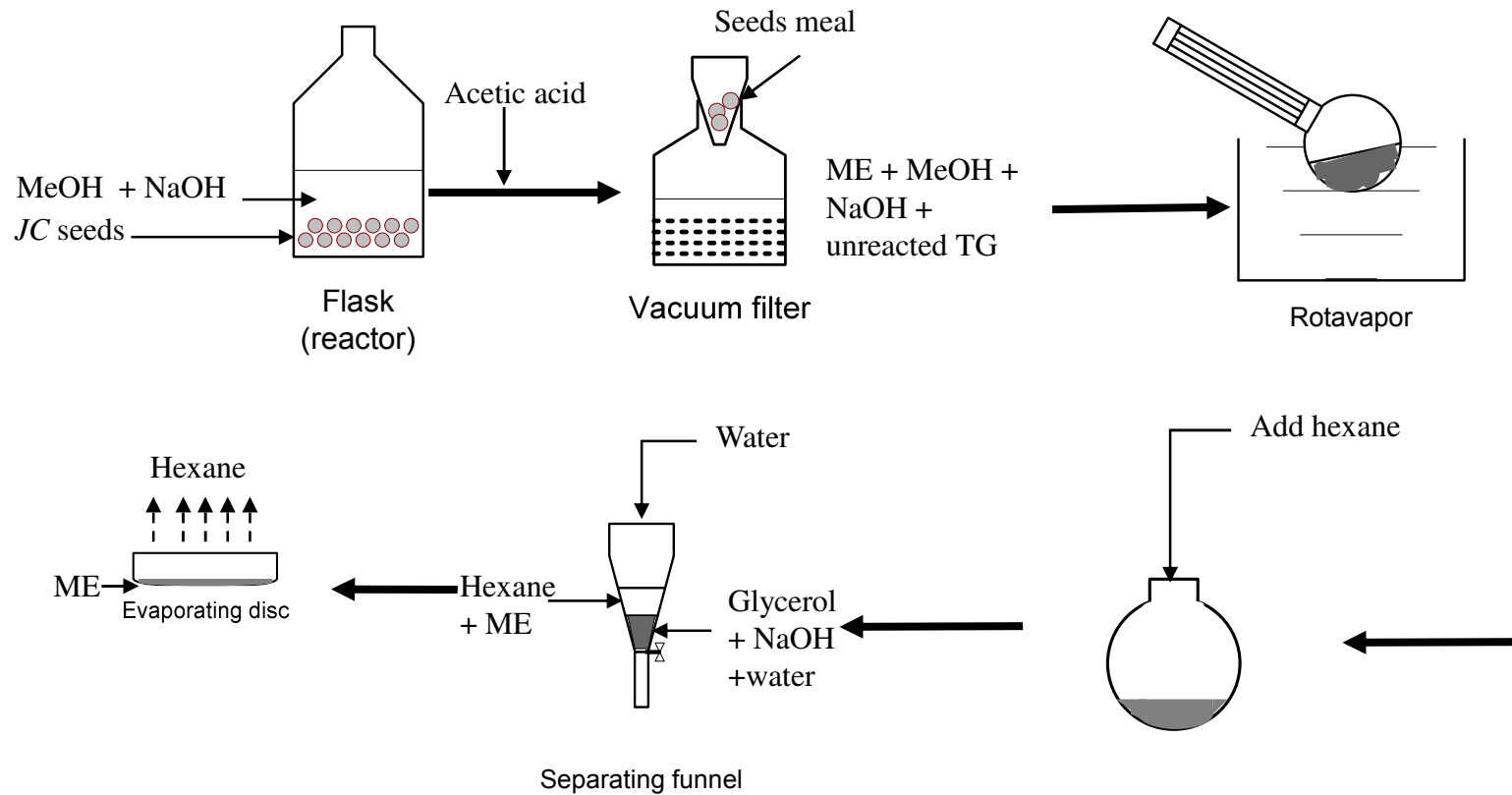


- Conventional transesterification of oil-bearing materials.



- In situ transesterification is the direct transesterification of ground oil-bearing materials.





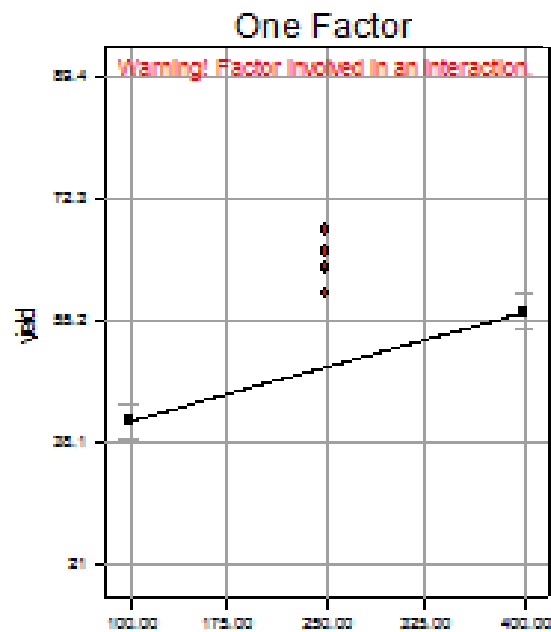
| Factor | Unit | Code | Level | |
|--------------------------------|------|------|-------|-----|
| | | | -1 | +1 |
| Molar ratio of methanol to oil | - | A | 100 | 400 |
| NaOH concentration | N | B | 0.1 | 0.2 |
| Reaction time | Min | C | 10 | 60 |
| Reaction temperature | °C | D | 30 | 60 |
| Mixing speed | rpm | E | 100 | 400 |

Two level factorial design

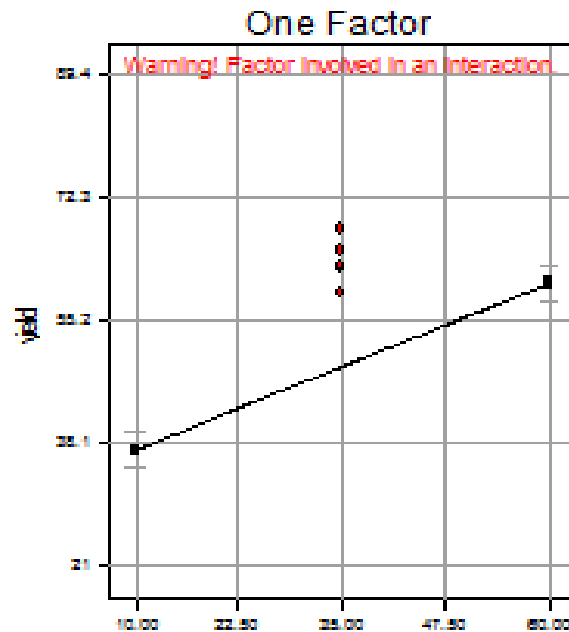


- Executed on Design Expert software
- Model used was a 2^5 full factorial design
- Model based on first order model
- 5 central points were added to the design to assess the experimental error and also the curvature
- Overall there were 37 experiments

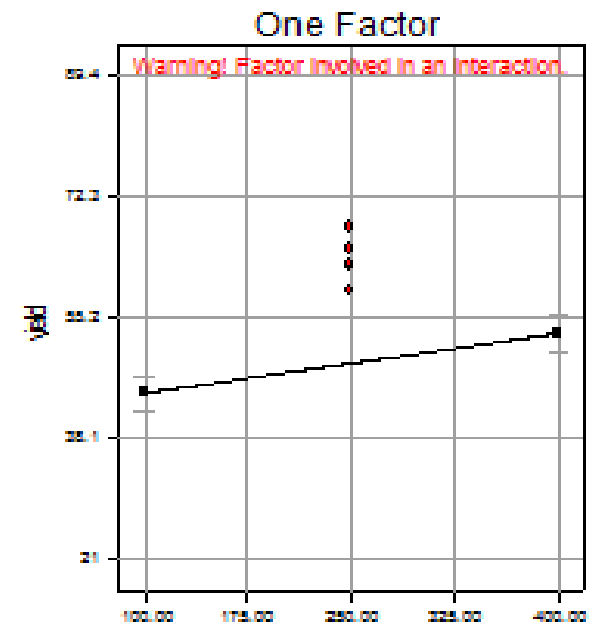




A: A



C: C



E: E

B= [NaOH]

D=temperature

A=molar ratio

C= reaction time

E=mixing speed

Methyl ester

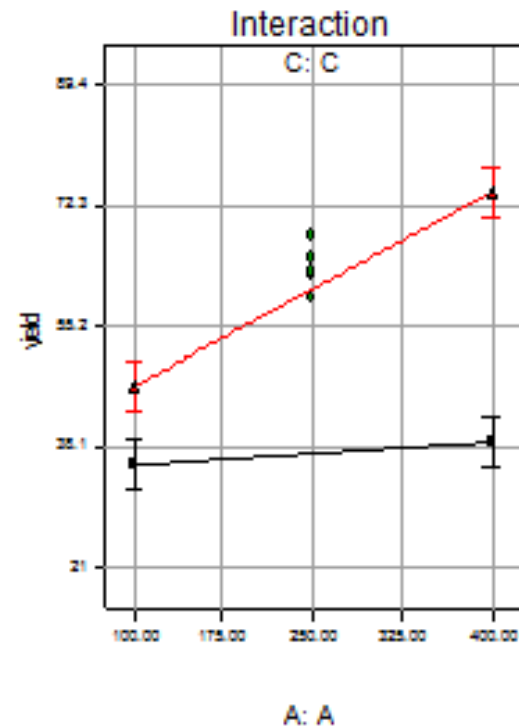
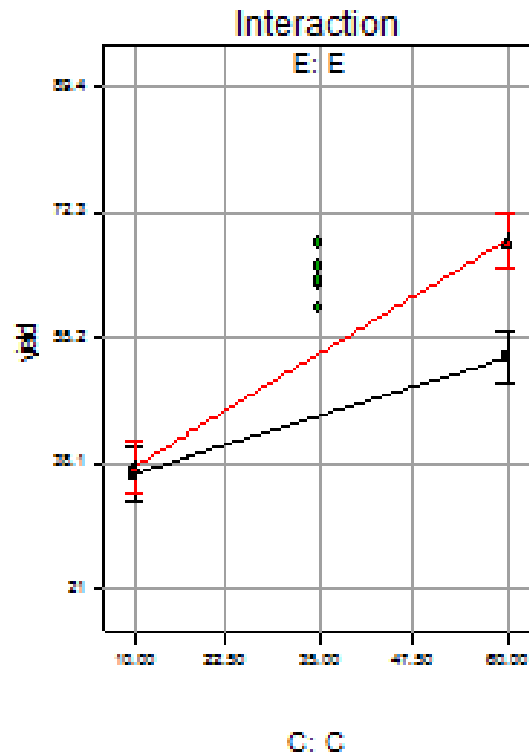
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Methyl ester

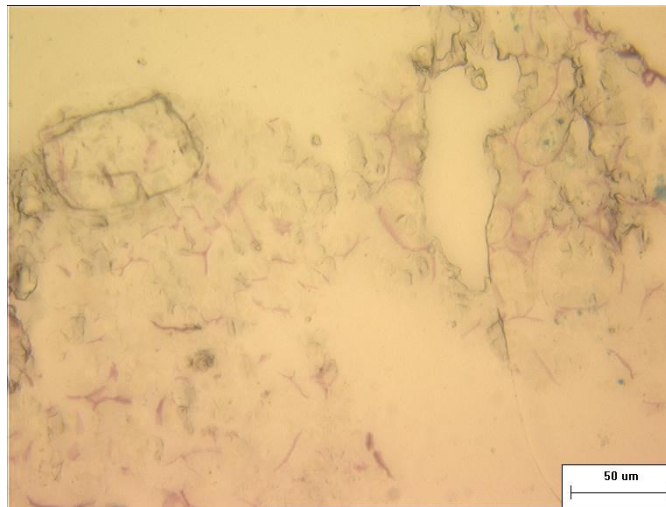
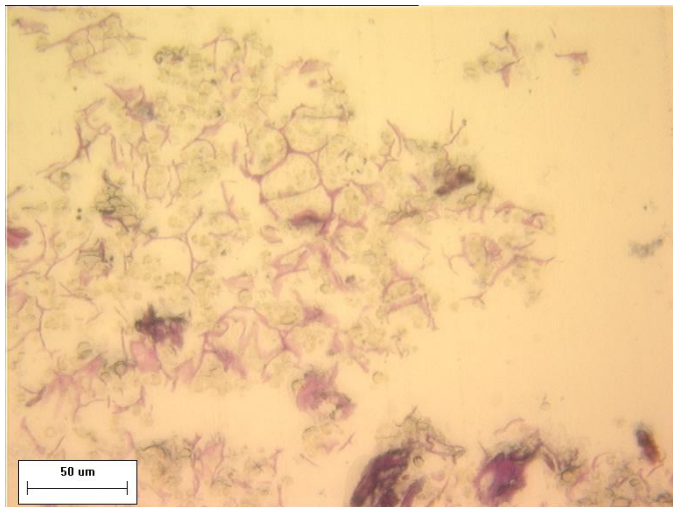
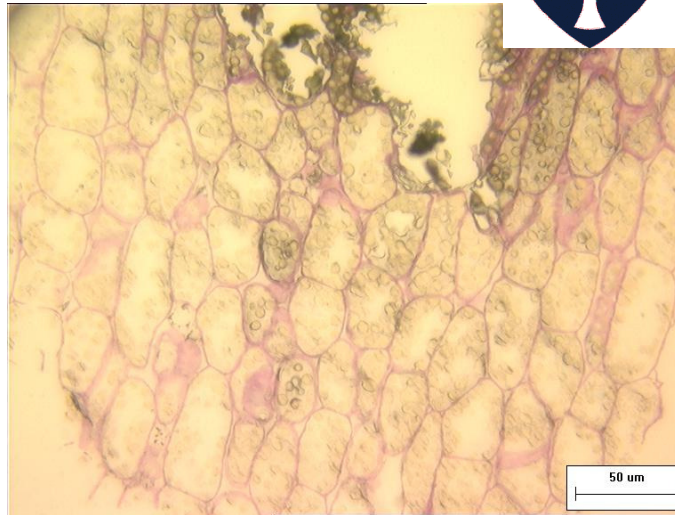
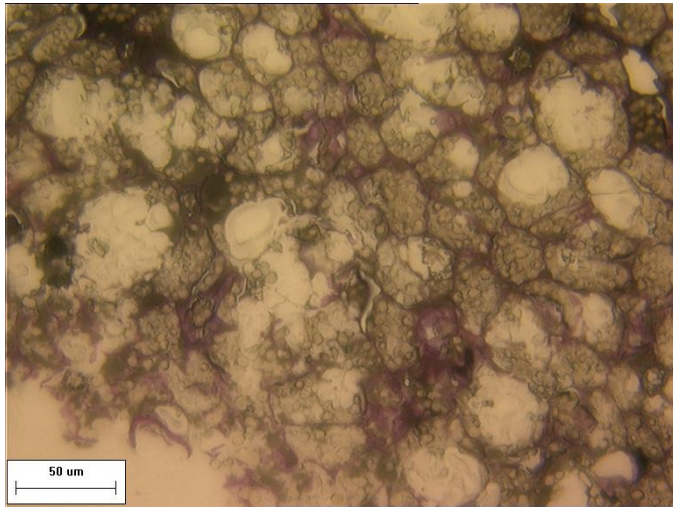
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Clockwise
from top:
Before
reaction, 100
molar, 300
molar, 500
molar

Methyl ester

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QuickTime™ and a
TIFF (Uncompressed) decompressor
are needed to see this picture.

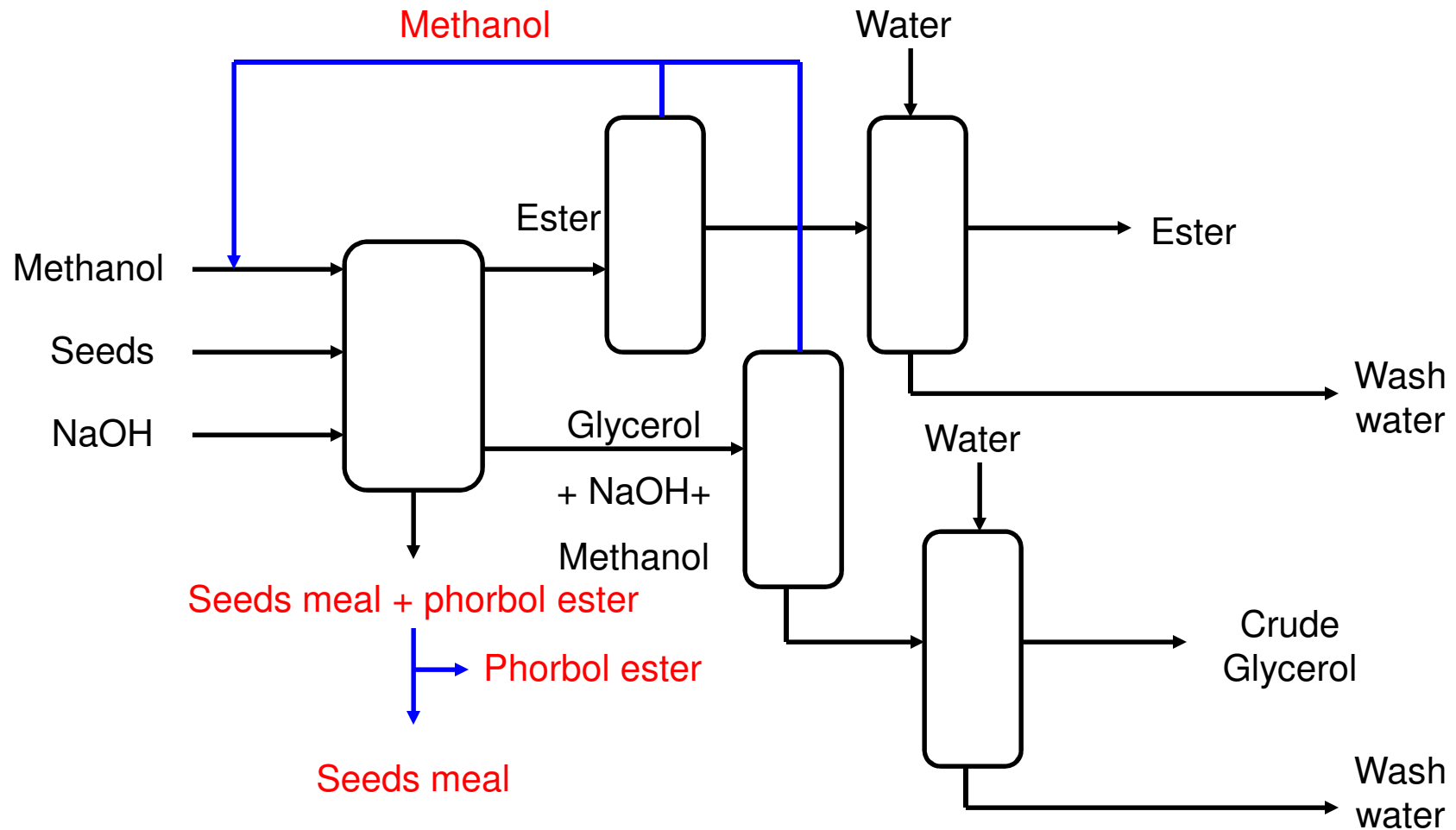
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Before Reaction

After Reaction



Next: Biorefinery concepts?



- A (molar ratio), C (reaction time) and E (mixing speed) are significant to the biodiesel yield
- B (catalyst concentration) and D (reaction temperature) are not significant to the biodiesel yield
- Interaction between A/C and C/E also significant to the yield
- The presence of curvature also significant, indicating that first order model is not suitable to predict the model
- Higher order model is needed to predict the model more accurately
- Optimal condition within this parameter space are:
 - 60 minute reaction time
 - 400 rpm agitation speed
 - 45°C reaction temperature
 - 0.17 N of NaOH concentration, and
 - 400 molar ratio of methanol to oil





Indian Institute of Petroleum

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